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(54) Method for the preparation of arylethylamines

(57) Arylethylamines are obtained by electrolytic reduction of the corresponding aryl nitroethene in the presence of a hydroxylamine in the catholyte using a strong negative cathode potential during the entire process.

SPECIFICATION

Method for the preparation of arylethylamines

5 This invention relates to an improved method of electro-chemically reducing 1-aryl-2-nitroethenes to arylethylamines.

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Although the electrochemical reduction of nitrostyrenes has been described in the chemical literature (cf for instance Japanese Patent 49-13777), the use of this technique as a practical preparation of phenylethylamines has seldom been realised because of insufficient chemical efficiency.

10 It has now been found that a method for preparing arylethylamines in water solutions in high yields and with excellent purity can be achieved.

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This new method is characterized by electrochemical reduction of a 1-aryl-2-nitroethene of the formula

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20 I R1

wherein Ar is an aromatic group, X is hydrogen or one or more substituents on the aromatic group selected from alkyl, alkoxy; hydroxy,

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 $(R^3 \text{ and } R^4 \text{ are the same or different and each representing hydrogen or alkyl), -N=(CH₂)_n (n=4,5,6),$

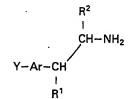
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45 -CN, -COOR³, -CF₃, -NO₂ and halogen, R¹ is hydrogen or methyl and R² is hydrogen or an alkyl group with 45 1-4 carbon atoms, in the presence of hydroxylamine or a salt thereof and with a strong negative cathod potential during the entire process to form an arylethylamine of the formula

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or a pharmaceutically acceptable salt thereof, in which formula Ar, R^1 and R^2 have the meaning given above and Y is as defined for X with the exception that it does not represent $-NO_2$.

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The arylethylamines have the general formula

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wherein Ar is an aromatic group, Y is hydrogen or one or more substituents in the aromatic group selected from alkyl, alkoxy, hydroxy.

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 $(R^3$ and R^4 are the same or different and each representing hydrogen or alkyl), -N

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-CN, -COOR3, -CF and halogen, R1 is hydrogen or methyl and R2 is hydrogen or an alkyl group with 1-4 carbon atoms.

Aromatic groups of interest in this Application are for instance phenyl, naphthyl or indolyl.

Alkyl groups of interest in this Application are straight or branched alkyl groups with 1-5 carbon atoms, for 35 instance methyl, ethyl, n-propyl and isopropyl.

Alkoxy groups of interest in this Application are alkyl-O- groups where the alkyl moiety is defined as above. Halogeno groups of interest in this Application are chloro, bromo and fluoro.

The phenylethylamines of formula I obtained by the method of the invention can be in the form of 40 pharmaceutically acceptable salts e.g. a hydrobromide, hydrochloride, phosphate, sulphate, citrate or

The compounds of formula I are useful as pharmaceuticals. The nitroarylethenes used as starting material in the process of this invention have the formula

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wherein Ar, R¹ and R² have the meaning given above and X is as defined for Y but can also represent +NO₂. The catholyte may consist of a dilute aqueous solution of a strong acid alone or a mixture of a strong acid,

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water and an organic solvent. The strong acid is for example sulfuric, hydrochloric, hydrobromic, phosphoric or a sulfonic acid. The concentration of acid and organic solvent if the later has acid-base properties should be such that the hydronium ion concentration is between 10^{-5} M and 20 M, preferably more than 10^{-3} M. The relative amounts of water and organic solvent can be varied over a wide range. The organic solvent may be an alcohol, carboxylic acid, ether, amide or nitrite. The ratio between catholyte volume and cathode area

should be as small as possible. The analyte may consist of diluted aqueous mineral acids, preferably sulfuric or hydrochloric acid. The concentration is from 2% to 10% by volume.

The anode is normally a DSA®-anode (metal anode overlaid with noble metal oxides) but may also consist 65

of lead, lead dioxide, graphite or platinum metals.

The cathode material must be carefully chosen. It must have an electrode surface with high hydrogen overpotential. This is achieved by making the cathode of a material with high hydrogen overpotential or by electrodeposition of a metal with high hydrogen overpotential on the cathode before or during the process.

5 The cathode material may be zinc, lead, cadmium, mercury, tin, or conducting materials (for example graphite, lead, nickel, copper, aluminium, titanium) on which deposition of for example zinc, lead, cadmium, tin or mercury can be done.

The electrolytic cell should be a divided one with good mass transport properties. The diaphragm can be of the ion exchanging type or a plastic tissue.

The temperature should be as low as possible. The process is usually carried out at temperatures below 20°C.

Cathode potential, current density, concentration of nitrostyrene and mass transport properties to the cathode surface are a function of each other. According to the invention it has been found that a large negative potential is important to carry out the reduction successfully. Therefore the reduction should be

10

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TABLE 1

	Chemic- a! effic- iency.	99	80	.08	98	. 62	81	74	74	72	79	76
	Amp. hours	45.8	.	2	49	79	42	45.5	4.2		E	4.2
	Current Potential ^{e)} density VISCE Aldm²	-1.55→-2.00		~1.60→-1.80	-1.60-→-1.90	-1.55-→1.90	-1,40->-1,46	-1.72→-1.90	-1.65→-1.53	-1.401.47	-1.25→-1.42	-1.28→-1.42
	Current density Aldm²	15	2	35	*		10.8	35	10.8	27.5	10.8	2
	Cathode	Pb			2	2			Graphite	Po	2	
٠	Temp. °C	16	2	23	2	2	16	23	16	. 52	16	E
	Н	100 0.2	2	Þ	2	ŧ	Þ	t	*	u		· f
	r mg	100	ŧ			2		200	100	£	×	£
	ns Metal salt	ZNCO3		t	•	ŧ	=	=	*	E		Þ
	conditio		0.018	£.	0.09	=	ŧ	0.036	0.018	*	=	
	Catholyte conditions Hydroxyl amm. salt mols	1	(NH ₂ - OH) ₂ H ₂ SO ₄	ŧ	t	£	0.018		2	t	E	(NH ₂ - OH) ₂ H ₂ SO ₄
	Ē,	9	*	~			*	12	9	ŧ	15	.
	Acid o	H ₂ SO ₄	£	E	E	E	E	z	*			E
	Cosolvent											
		ro '	•.	•	•	•	•	,	ر ب	•	•	•
	H ₂ O	105		t	=		=	210	105	Ė	92	80
	Sub- strate mols	0.05			•	0.14	0.0045	0.05	0.0045	*	e	
	Run no.	_	2	က	4	2	9	7	œ	တ	10	=

TABLE 1 (cont...)

Amp. Chamic- hours al effic- iency %	78		98		8 &	. 19	
Amp. hours	4.2		11.1	5	=	20.4	
Current Potential ^{e)} density VISCE Aldm²	15→12.5 ^{a)} −1.6 ^{d)}		- ≈-2.1		ı	13.5 -1.20→-1.70	
	15		С	15		13	
Cathode	Pb			÷		t	
Ca mg pH °C	16		2	2			
На	0.4		2				
t mg	100		=	=	2		
letal sa	ZnCO ₃ 100 0.4 16		=	z	E	a)	
condition mols			0.008	=	2		
Catholyte conditions Hydroxyl M amm. salt mols	,	(NH ₂ OH) ₂	4.1 H ₂ SO ₄	E	2	ı	
<i>j</i> w	വ			9	Ħ	3r20	
Acidel	豆		H ₂ SO ₄	2	2	40% HBr20	
Cosolvent			MeOH 89	EtOH 60	i-PrOH"	МеОН 87	
H ₂ O	100		17	45	÷	22	
Sub- strate mols	0.0045		0.014	E	=	0.032	i
Run no.	12		13	14	15	16 ^{b)}	•

Zinc was electro-depositioned on the cathode surface before the nitrostyrene reduction.
The conditions according to Japanese Patent 49-13777.
The acid volume before the electrolysis.
Constant potential electrolysis.
The arrows show the changes during the electrolysis.

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Example 2

The same equipment was used and the experiments were run in the same manner as in example 1.

TABLE 2

Amp. Chemic- hours al	iency .%	09	18
Amp. hours		15.8	*
Current Cathode density potential ^{b)}	Aldm² VISCE	-1.50→-1.54 15.8	-1.49→1.55
Curren density	A/dm²	13.5	=
Cathode		Pb	n n
Temp. °C		16	\$
alt	тд	100 16	
tions Metal salt		ZnO	
conditic	spom		0.012
Catholyte conditions Hydroxyl amm. salt		•	(NH ₂ OH) 0.012 H ₂ SO ₄
)E	22	2
Sosolvent Acid ^{e).}		달	=
solvent	/w	MeOH 87	=
•			=
H ₂ O		27	=
Sub- strate mols		0.0106	2
Run no.		_	8

a) The acid volume before the electrolysis.b) The arrows show the changes during the electrolysis.

The same equipment was used and the experiments were run in the same manner as in example 1.

	Chem- ical	iency %	. 08	22	70
	Amp. hours		27.8	=	z
	Current Cathode density potential ^{b)}	A/dm² V/SCE	≈-1.52	-1.0→-1.1	≈-1.5
	Curren density	A/dm²	13.5	വ	13.5
	Cathode		Pb	2	2
	Тетр	ပ့	16	•	E
		J。 bu	100 16	E	*
			ZnO	t	٤
	conditi	slom	0.012	ŧ	
TABLE 3	Catholyte conditions Hydroxyl amm.Metal salt salt		(NH ₂ OH) ₂ 0.012 ZnO H ₂ SO ₄	2	ı
Τ	droxyl	<i>Ju</i>	22	"	t
	Ħ		H	ž.	ŧ
	4 <i>cia</i> e)	<i>Ju</i>	MeOH 87	£	*
	H ₂ O CosolventAcia ^{c)} ml		_		*
			27	*	
	Sub- strate mols		0.0106	E	
	Run No.		-	7	ო

The same equipment was used and the experiment was run in the same manner as in example 1.

TABLE 4

Run no.

Ė.						
	Chem- ical effic- iency %					
Amp. hours		27.8				
Current Cathode density potential	A/dm² V/SCE	13.5 -1.32-1.38				
Curre	A/dm	13.5				
Cathode		Pb				
Temp. °C		16				
	mg	100 16				
ons Metal salt		ZnO				
conditi	mols	0.004				
Catholyte conditions Hydroxyl amm. salt		(NH ₂ OH) ₂ 0.004 H ₂ SO ₄				
	lm/	. 22				
Aciao		<u>I</u>				
Cosolvent Acid ^{e)}	/w	MeOH 87				
H ₂ O		27				
Sub- strate	mols	0.0024 27				

The experiment was run as in example 1 except that the anolyte consisted of 90% ethanol and 10% concentrated sulfuric acid.

TABLE 5

Run no.

; ;	_				
Chem- ical effic-	82				
Amp. hours	Amp. hours				
Current Cathode density potential	Aldm² VISCE	-1.8 -4.0			
Currer	A/dm²	12.5			
Cathode		Pb			
Temp. °C		23			
بي	mg	300			
nns Metal salt		ZnSO4			
conditie	sjom	0.02			
Catholyte conditions Hydroxyl amm. salt		(NH ₂ OH) ₂ (H ₂ SO ₄			
	m/	10			
Acidel		를 단			
Cosolvent	Jm	MeOH 175			
H ₂ O		15			
Sub- strate	slow	0.25			



The experiment was run as in Example 5.

Run no.

	Chem- ical	iency %	82
	Amp. hours	45	
	Current Cathode density potential	V/SCE	12.5 -1.8 -4.5
	Current density	Aldm²	12.5
	Cathode		Pb
	Temp.	ပ္	24
	ų.	mg	300 24
	ons Metal salt		ZnSO ₄
	onditi	sjou	0.02
ABLE 6	Catholyte conditions Hydroxyl	amm. salt	(NH ₂ OH) ₂ 0.02 H ₂ SO ₄
Ţ		<i>J</i> w	9
	Acid ^{c)}		HC
	Cosolvent	<i>Ju</i>	MeOH 175
	H ₂ 0	<u>3</u>	15
	Sub- strate	mols	0.25

The same equipment was used and the experiment was run in the same manner as in Example 1.

	Chem- ical	effic- iency	, , , , ,
	Amp. hours		10
	Current Cathode density potential	VISCE	-2.0 -3.0
	Curren densit,	Aldm ²	12.5
	Cathode		원
	Temp.	د	30
	٠.	mg	100
	ons Metal salt		ZnSO ₄ 100 30
	conditi	spom	0.01
ABLE 7	Catholyte conditions Hydroxyl amm. salt		(NH ₂ OH) ₂ 0.01 H ₂ SO ₄
¥.		<i>]</i>	25
	Acidel		HCI
	Cosolvent	<u>/</u> E	МеОН 90
	H ₂ O		32
	Sub- strate mols		0.1
	Run no		



The experiment was run as in Example 1, except that the analyte consisted of 60% THF and 40% 1 M H₂SO₄.

	Chem- ical	effic- iency	% 08 % 08
	Amp. hours		6.7
	Current Cathode density potential	Aldm² VISCE	10
	Cathode		Pb
	Тетр.	ပ္	
	*	тв	36
	ns Metal salt		0.006 ZnCO ₃
	onditio	slow	900.
TABLE 8	Catholyte conditions Hydroxyl Met	amm. salt 1	(NH ₂ OH) ₂ (H ₂ SO ₄
TAE		<i>[u</i>	ro O
٠	Acide		H ₂ SO ₄
	Cosolvent	ju	99
,	Cosol	· .	井
	H ₂ O)E	32
	Sub- strate	mols	0.005
	Run no.		

Example 9

The experiment was run as in Example 8.

	Chem-	ical effic-	iency %	.06
	Amp.	4		
	Cathode Current Cathode	density potential	Alulii VISCE	- 01
	Cathode	P		
		Temp.	د	31
			mg	96
	su	Metal salt		ZnCO3
	conditio		mols	900.0
TABLE 9	Catholyte conditions	Hydroxyl		5 (NH ₂ OH) ₂ 0.006 ZnCO ₃ 36 31 H ₂ SO ₄
Ĭ			m/	D.
		Acidel		H₂SO₄ 5
		vent	/ш	09
		Cosolvent		표
	H ₂ 0	/m		32
	Sub-	strate mols		
	Run	<i>no.</i>	-	•

CLAIMS

1. A method for the preparation of an arylethylamine of the formula

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R²
I
CH-NH₂
Y-Ar-CH

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or a pharmaceutically acceptable salt thereof, in which formula Ar is an aromatic group, Y is hydrogen or one or more substituents in the aromatic group selected from alkyl, alkoxy, hydroxy,

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25 (R^3 and R^4 are the same or different and each representing hydrogen or alkyl, -N (CH_2)_n (n = 4,5,6),

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-CN, $-COOR^3$, $-CF_3$ and halogen, R^1 is hydrogen or methyl, and R^2 is hydrogen or an alkyl group with 1-4 carbon atoms comprising electrochemical reduction of a nitrostyrene of the formula

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wherein Ar, R^1 and R^2 have the meaning given above and X is as defined above for Y but additionally can also represent $-NO_2$, in the presence of hydroxylamine or a salt thereof and with a strong negative cathode potential during the entire process.

- 2. A method according to claim 1 wherein Ar is a benzene, naphthalene or indene residue.
- 3. A method according to claim 1 or 2 wherein X is dimethylamino, methyl, hydrogen, hydroxy or methoxy.

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- 4. A method according to any one of the preceding claims wherein R¹ is hydrogen.
- 5. A method according to any one of the preceding claims wherein R² is hydrogen, methyl or butyl.
- 6. A process according to claim 1 comprising reduction of a nitrostyrene of the formula

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$$CH_3 = C + CH = C + CH_3$$

$$CH_3 = CH_3$$

$$CH_3 = CH_3$$

$$CH_3 = CH_3$$

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to a phenethylamine of the formula

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7. A method according to any one of the preceding claims wherein the catholyte comprises aqueous acid.

8. A method according to claim 7 wherein the hydronium ion concentration in the catholyte is 10^{-5} M to 20M.

9. A method according to claim 7 or 8 wherein the catholyte comprises an organic solvent.

10. A method according to claim 9 wherein the solvent is methanol, ethanol, isopropanol or tetrahydrofuran.

11. A method according to any one of the preceding claims wherein the catholyte comprises more than 15 0.1 M hydroxylamine or a salt thereof.

12. A method according to any one of the preceding claims wherein the anolyte comprises 2-10% by volume sulphuric acid or hydrochloric acid.

13. A method according to any one of the preceding claims wherein the cathode is lead.

14. A method according to any one of the preceding claims wherein a negative potential more negative than 1 volt, relative to a standard calomel electrode, is used.

15. A method according to claim 1 substantially as hereinbefore described with reference to any one of the Examples.

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